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CO₂ Absorption and Precipitation in MgCl₂-NH₃ · H₂O Solutions: Relevance to CO₂ Sequestration

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Mineral sequestration of CO₂ is one of the safer options in the portfolio of available Carbon Storage and Sequestration (CCS) stratagems. To date, numerous approaches, such as MEA/DEA/Ammonia based post combustion scrubbing and O₂/CO₂ recycle combustion,

were tested to optimize the absorption of CO₂ using various media. These methods were shown to be able to achieve CO₂ capture, but did not address the costly issue of carbon storage. Following a newly proposed pH-swing CO₂ mineralization process (Kodama *et al.*, 2008) which

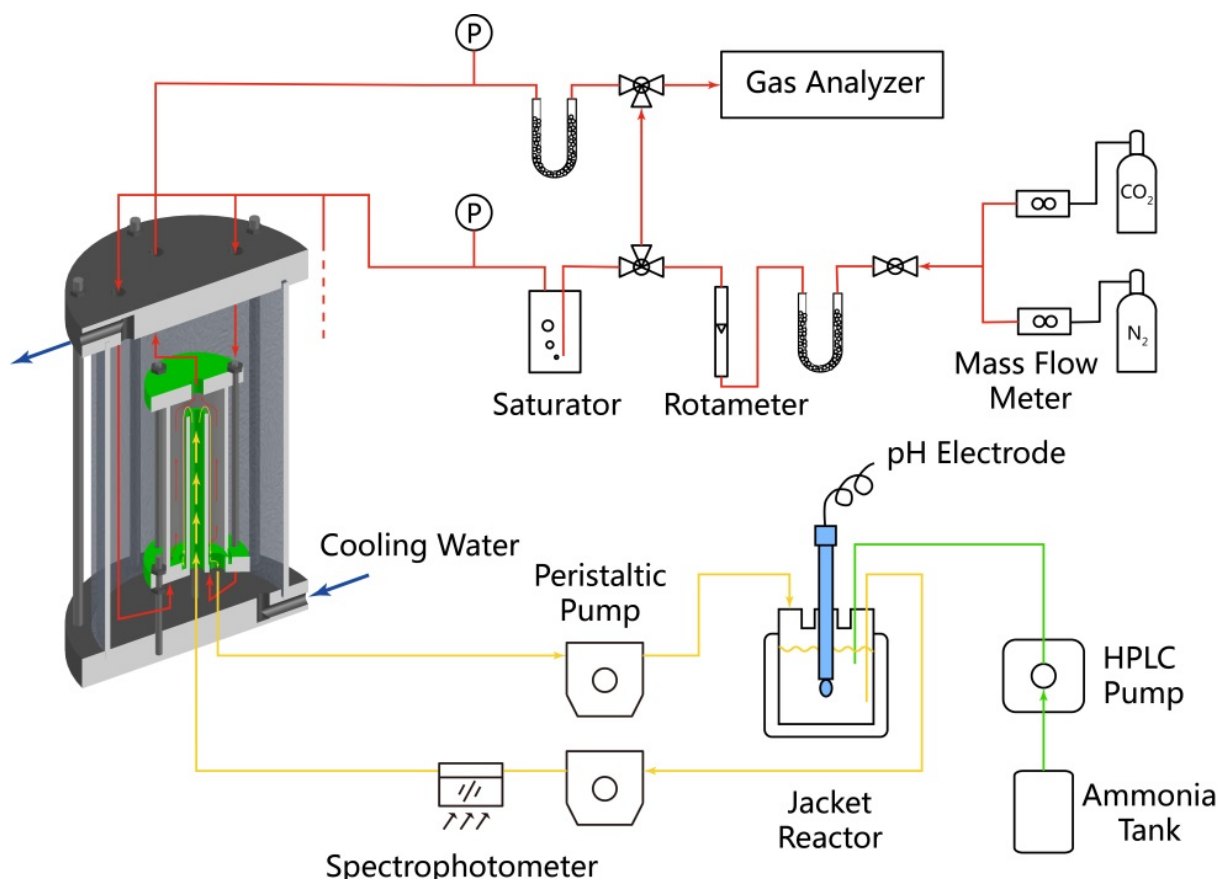


Fig. 1. Schematic diagram for the CO₂ absorption system

CO₂ absorption experiments were carried out at 298 K in solutions of different compositions (0.05–0.2 mol/L MgCl₂) to measure the reaction kinetics using a wetted wall column setup similar to those reported in Pacheco (1998) and Victor (2011). The solution chemistry was maintained at conditions where brucite precipitation was not allowed. The absorption solution was then cycled between the column and a jacketed glass reactor with its pH maintained constant, and the transmittance at 546 nm was monitored in real-time. Magnesium concentration was analyzed by ICP-AES with interval sampling.

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showed potential of being able to capture and store CO₂ simultaneously. we investigated the rate and kinetic controlling factors for CO₂ absorption and mineralization in MgCl₂-NH₃ solutions in this study to better understand the system behavior. CO₂ absorption experiments were carried out at 298 K in solutions of different compositions (0.05~0.2molL⁻¹ MgCl₂) to measure the reaction kinetics using a wetted wall column setup similar to those reported in Pacheco (1998) and Victor (2011). The solution chemistry was maintained at conditions where brucite precipitation was not allowed, and magnesium concentration was analyzed by ICP-AES with interval sampling. The absorption solution was then cycled between the column and a jacketed glass reactor with its pH maintained constant and the transmittance at 546 nm monitored in real-time. Preliminary results indicate that initial concentration of Mg in solution has little effect on CO₂ absorption. Although CO₂ absorption rate increased slightly over time with increasing ammonia addition, pH appeared to be the dominant controlling factor. The higher the solution pH was, the faster the absorption rate increased. Upon reaching saturation, nesquehonite precipitated as indicated by the decreased laser transmittance, leading to rapid addition of aqueous ammonia. However, precipitation of nesquehonite unexpectedly showed little influence on CO₂ absorption, suggesting that the interaction between aqueous CO₂ and

OH⁻ or ammonium ions in liquid film may be the rate limit step during the absorption process, further indicating that the gas-liquid interaction barrier should be treated seriously in order to optimize CO₂ capture efficiency. Due to the low gas-liquid reaction area (0.005 m²L⁻¹), extended time period (2~3 hours) was needed to dissolve enough CO₂ for nesquehonite to reach supersaturation. Measured typical absorption rates under these experimental conditions are between 0.000668 mol s⁻¹m⁻² (pH=8.74, pCO₂= 15495Pa, 298K) and 0.001997 mol s⁻¹m⁻² (pH=9.16, pCO₂= 15403Pa, 298K).

Key words: Nesquehonite, Carbon dioxide, Mineral carbonation, CO₂ sequestration

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